

# Experimental testing of an absorption-based heat store

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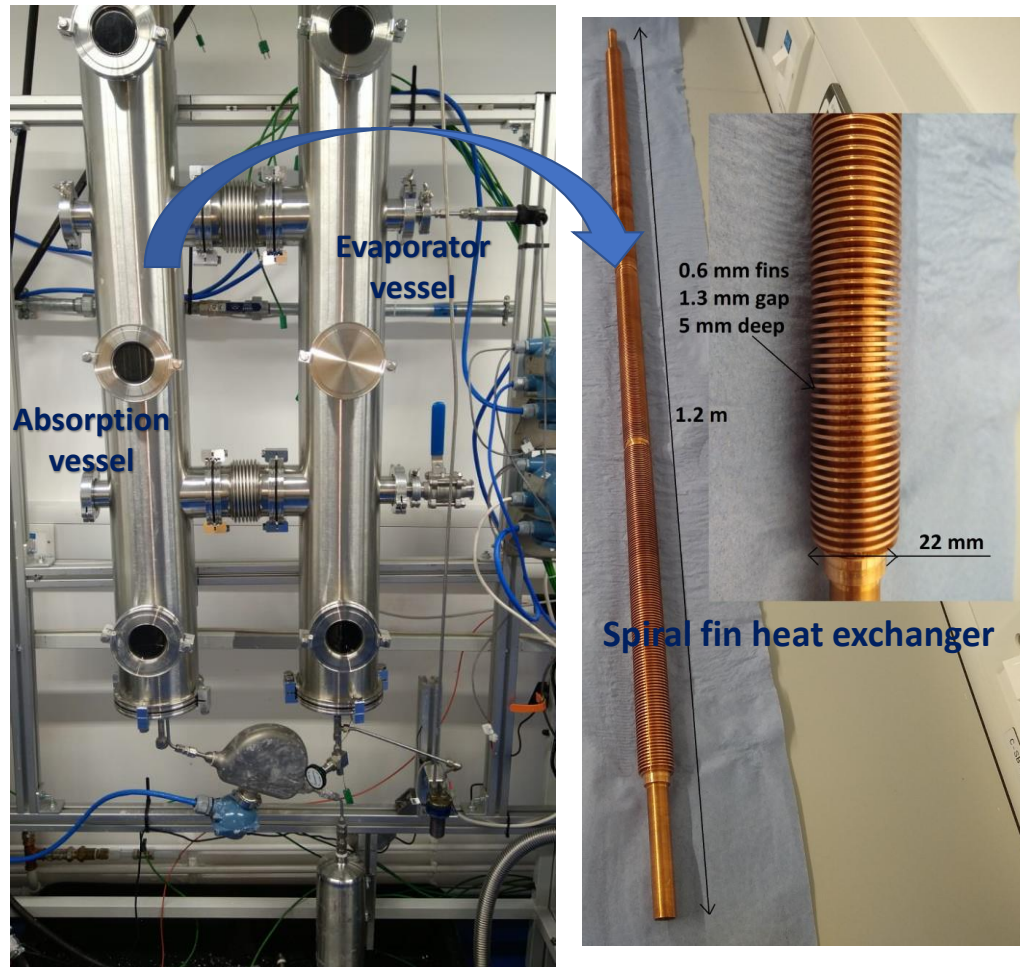
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## Motivation

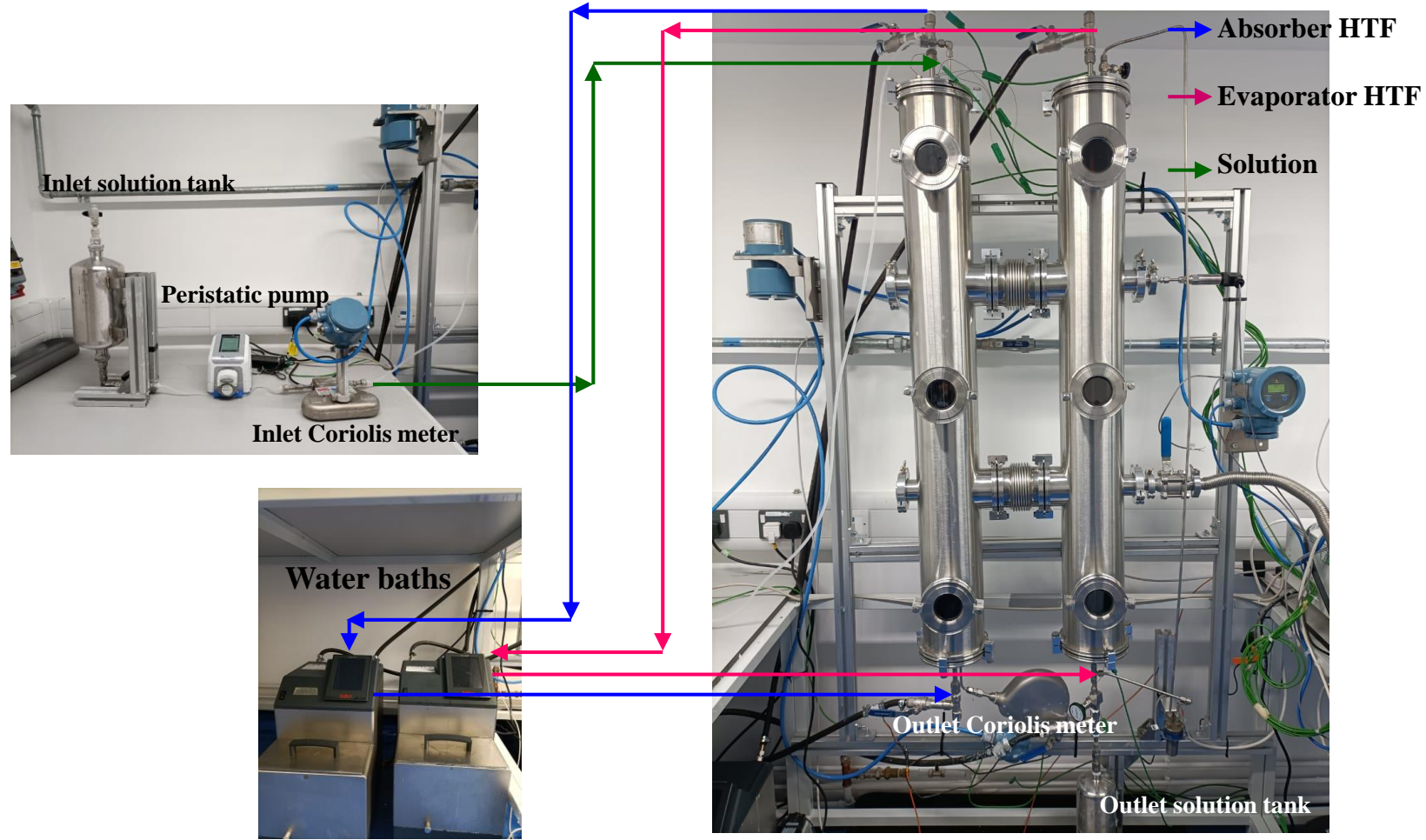
- Heating and cooling needs contribute 40-50% of global energy consumption, with over 40% for domestic applications.
- Thermal energy storage can play an important role in the renewable energy integration and peak load reduction in buildings.
- Thermochemical sorption storage systems are seen to offer among the highest energy storage densities ( $>1500 \text{ MJ/m}^3$ ).
- They enable storage at near ambient conditions and reduce heat loss.
- Solution based sorption materials are seen to offer better heat and mass transfer characteristics along with higher energy densities over the solid based ones.
- Among the various commonly used absorbents such as  $\text{LiCl}$ ,  $\text{LiBr}$ ,  $\text{CaCl}_2$ , etc.,  $\text{NaOH}$  has emerged as a potential sorbent with  $\text{H}_2\text{O}$  along with being less expensive.

## System description

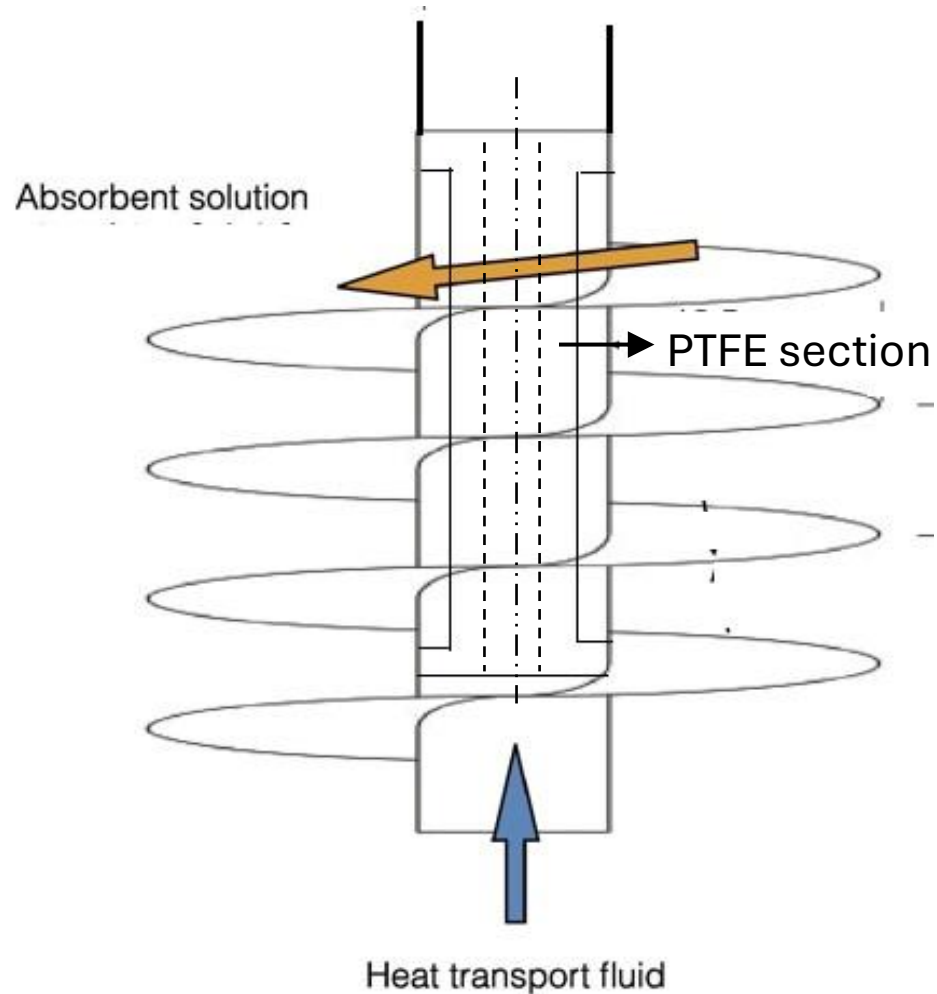


- NaOH-H<sub>2</sub>O pair studied for domestic heating applications.
- Absorption performance is evaluated over spiral finned heat exchangers.

# Test setup layout

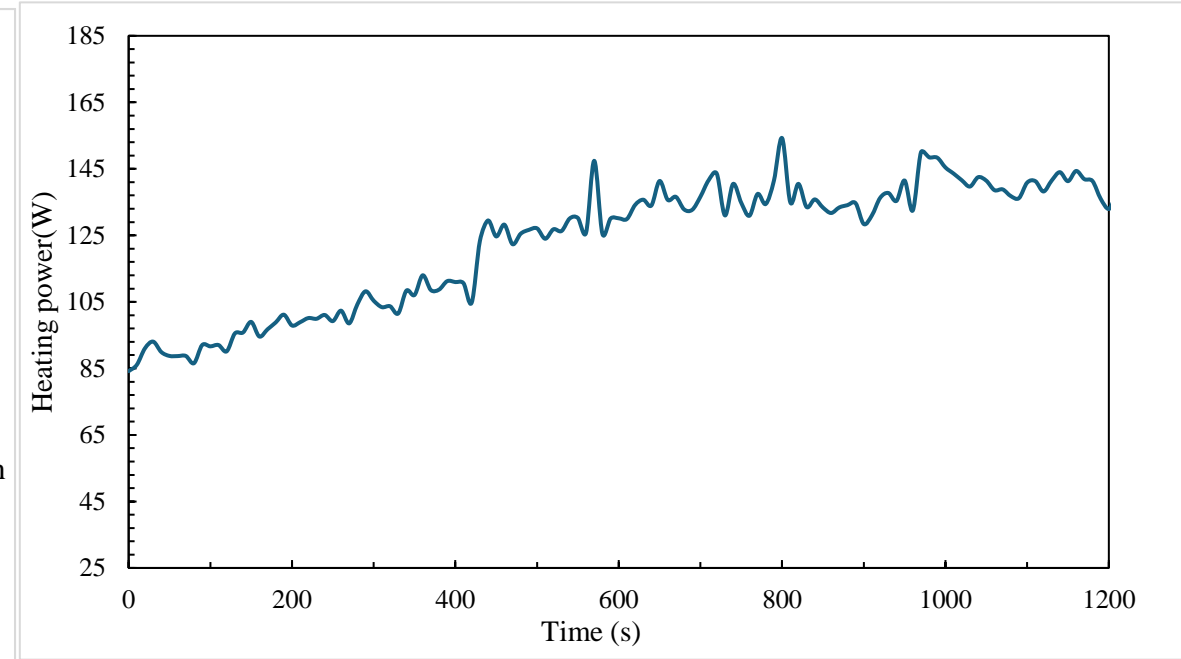
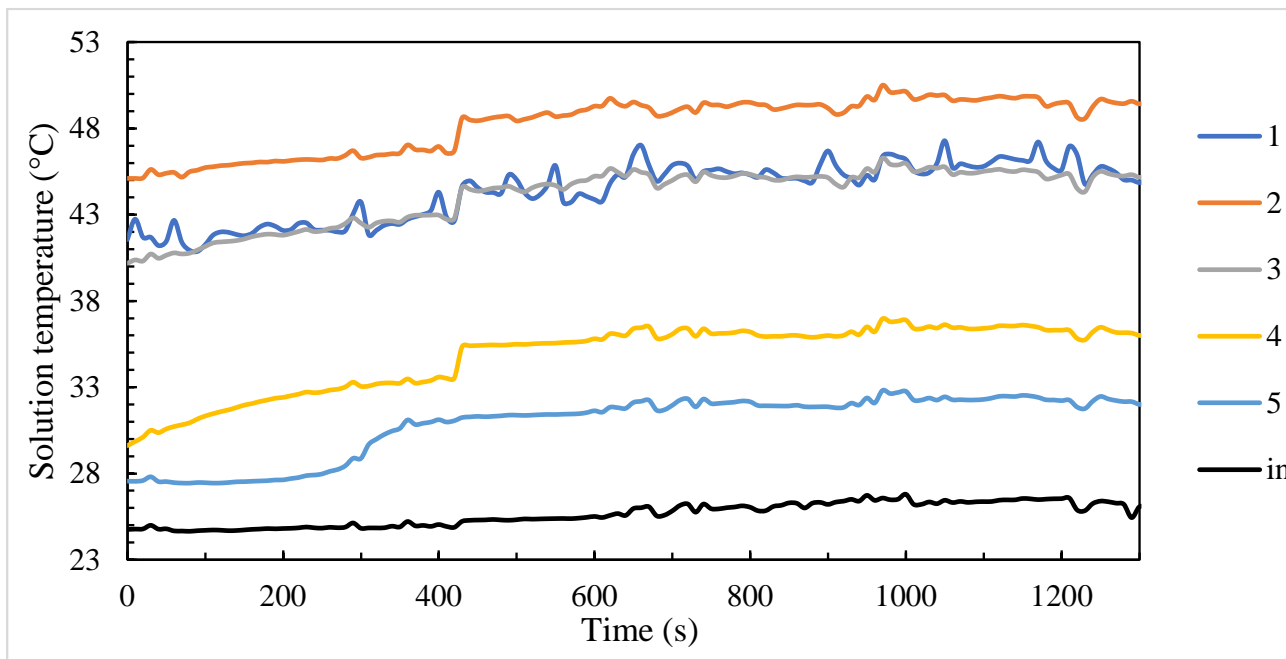


## Preheating section



- The PTFE insulating column of 15cms in length enables a temperature rise up to 20C.
- It leads to a reduction in the heat transfer area.
- The impact of the preheating section elimination is studied.

# Temperature and discharge power profiles



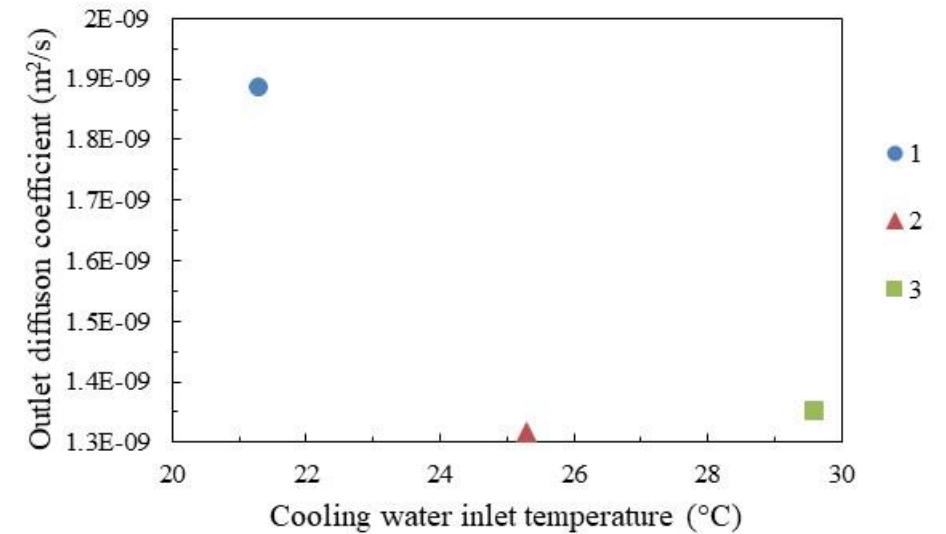
# Parametric studies

## Spiral finned heat exchanger specifications

Length (m)	Outer diameter (mm)	Pitch (mm)	Fin height (mm)
1.2	12.7	1.9	3

## Absorption performance with varying cooling water inlet temperatures

Case	Solution flow rate (g/min)	Cooling water inlet temperature(°C)	Heating power	Solution outlet concentration
1	5.8	21.3	150.7	30%
2	7.5	25.4	99.0	37%
3	6.5	29.6	69.9	39%





# Parametric studies (contd.)

## Impact of varying evaporator temperatures

Evaporator temperature (°C)	Solution flow rate (g/min)	Cooling water inlet temperature(°C)	Heating power (W)	Solution outlet concentration
20	6.2	27.9	141.4	31%
15.5	6.8	25.0	151.8	31%
11	6.0	21.3	150.7	31%
7	5.7	17.8	124.4	32%

## Impact of varying solution flow rates

Case	Solution flow rate (g/min)	Heating power	Solution outlet concentration	Average solution temperature (°C)
1	5.7	80.7	36%	34.4
2	7.5	99.0	37%	36.4
3	9	61.1	42%	32.3

## Heat exchanger specifications

- Nickel coated copper based spiral finned heat exchangers are considered for the solution absorption.
- While the evaporator vessel has a fixed heat exchanger, the heat exchangers of the absorption vessel have been varied for the parametric analysis.



Heat exchanger	Length (m)	Outer diameter (mm)	Pitch (mm)	Fin height (mm)
HEX 1	1.04	12.7	1.9	3
HEX 2	1.04	15.8	1.9	6.35

## Performance evaluation

The key non dimensional parameters of the heat and mass transfer are evaluated for the average temperature and concentration conditions of the solution.

$$Re = \frac{\rho_{avg} v d_h}{\mu_{avg}}$$

$$Sc = \frac{\mu_{avg}}{\rho_{avg} D_{avg}}$$

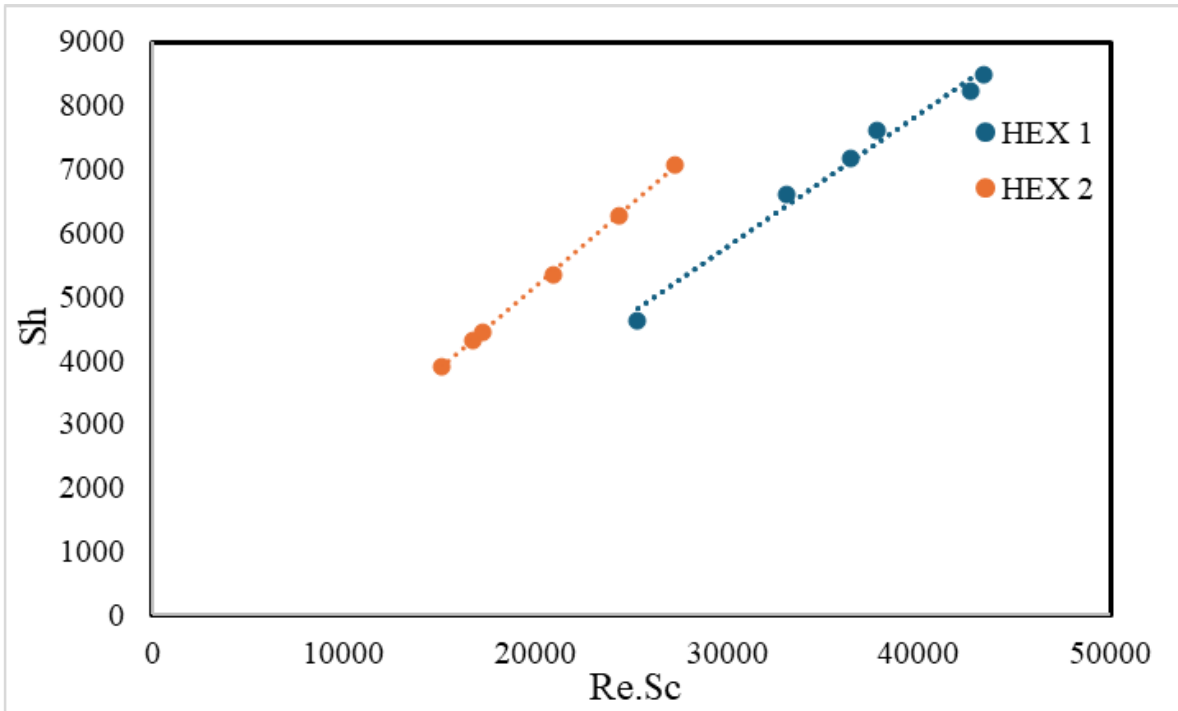
$$Sh = \frac{\dot{m}_v}{A(\rho_{in} - \rho_{out}) D_{avg}}$$

$$Q_{disch} = \dot{m}_w \times 4.18 \times (T_{w,out} - T_{w,in})$$

$$Storage\ density = \frac{Q_{disch}}{\dot{m}_{s,in}}$$

## Non dimensional characterization

The mass transfer parameter  $Sh$  is plotted against the product of  $Re$  and  $Sc$  to take into account both the inertial and diffusive components of the solution flow.

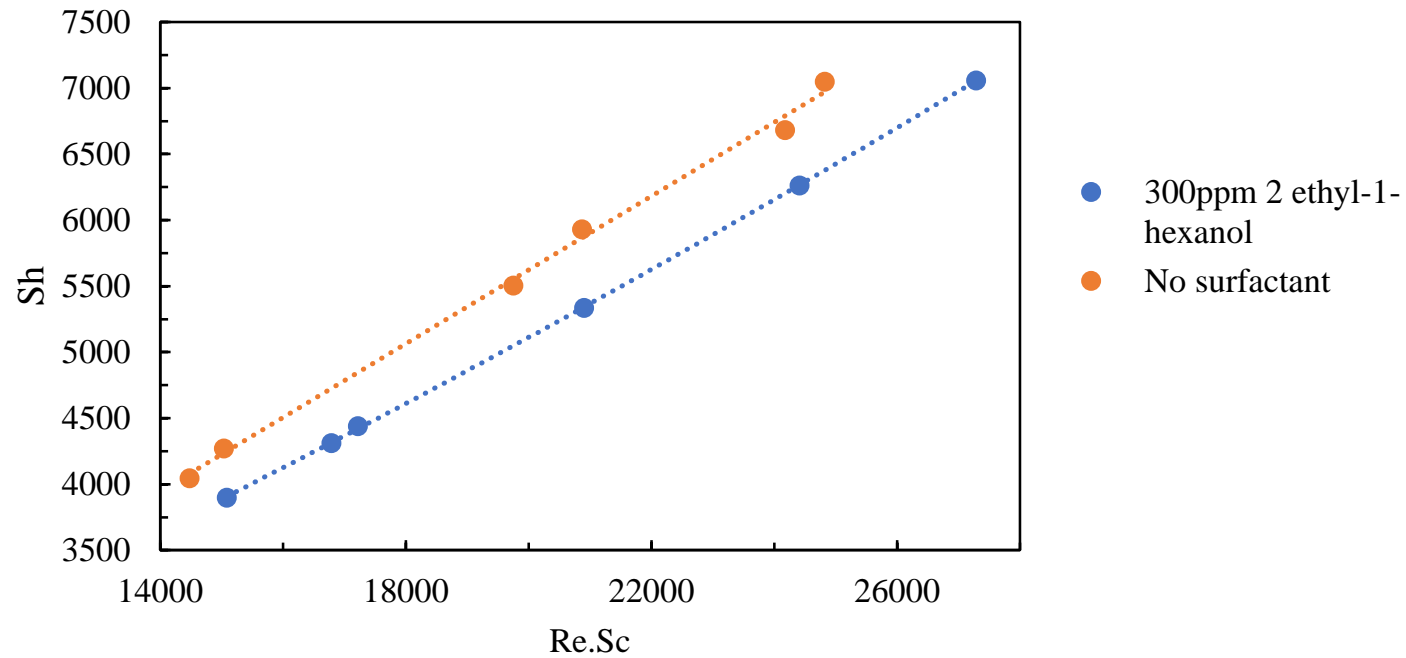


- A higher value of the product  $Re.Sc$  is observed for higher mass flow rates and lower evaporator temperatures.
- A lower evaporator temperature could be preferred over higher mass flow rate for higher storage density.
- HEX 1 outperforms HEX 2 for all the similar operating conditions and mass flow rates.
- The relatively lower  $Re$  number of the flow in HEX 2 is the primary reason for its lower  $Sh$  values.

## Impact of surfactants

Surfactant	Solution flow rate (g/min)	Cooling water inlet temperature(°C)	Discharge power	Solution outlet concentration
None	6.6	15.1	122.9	35%
1-Octanol 300 ppm	7.0	14.8	121.4	35%
1-Octanol 500 ppm	5.8	14.9	87.6	37%
2-Ethyl-1-Hexanol 100ppm	7.7	14.8	139.6	34%
2-Ethyl-1-Hexanol 300 ppm	6.9	14.8	151.1	33%
2-Ethyl-1-Hexanol 500 ppm	6.8	14.9	125.6	34%

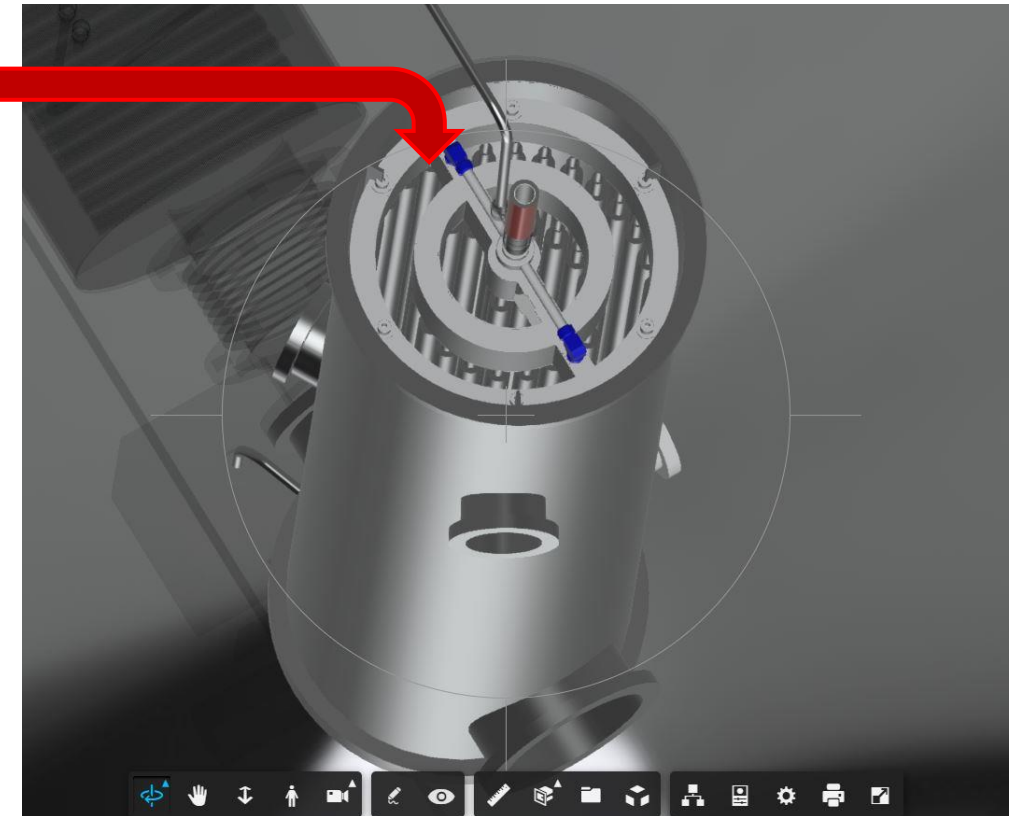
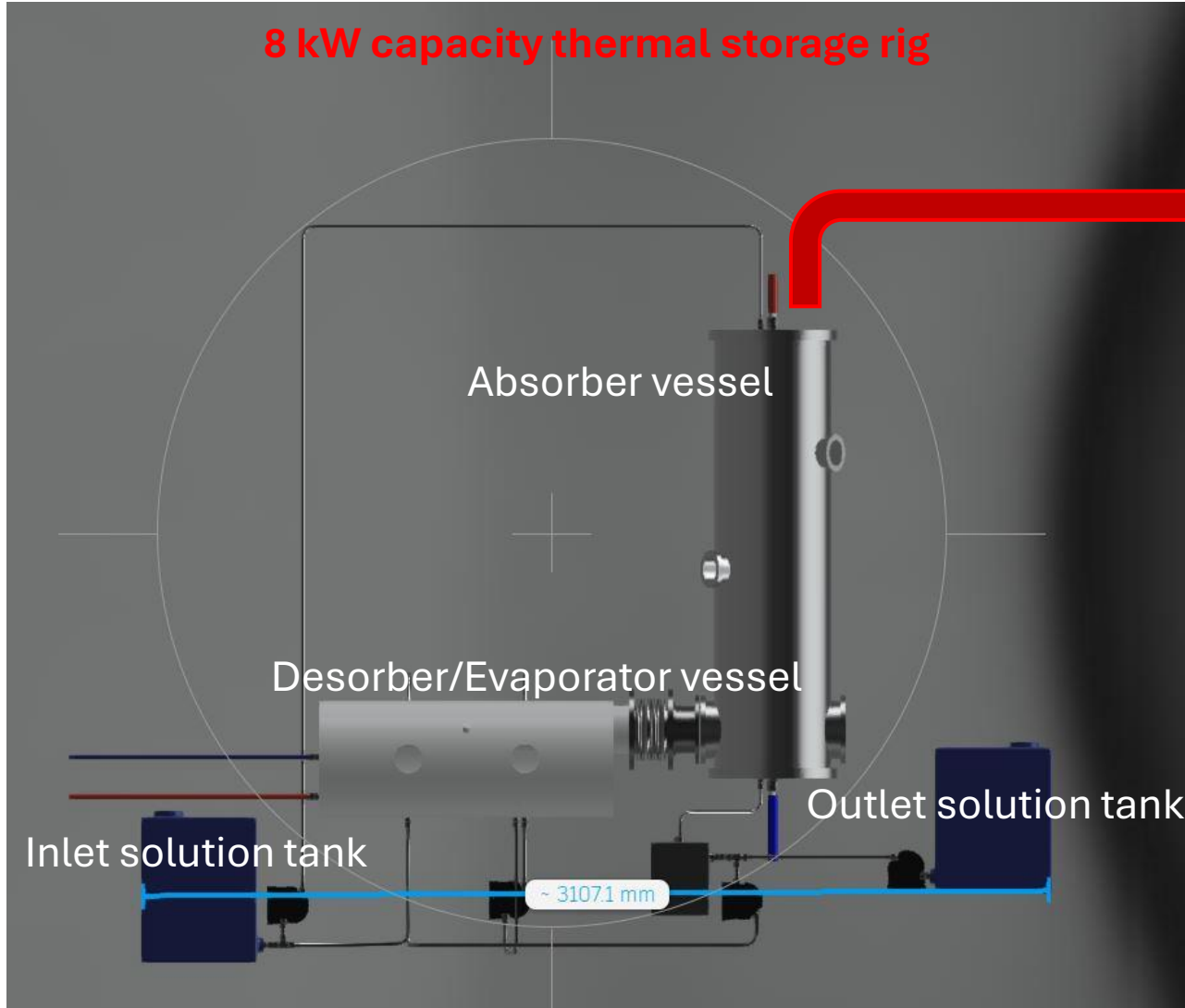
## Impact of surfactants (contd.)



- Higher values of  $Sh$  are observed with surfactant for all the similar operating conditions.
- Discharge power is enhanced by 16-20%.
- Surfactant is seen to enable better performance at lower solution flow rates and thus enables higher storage density

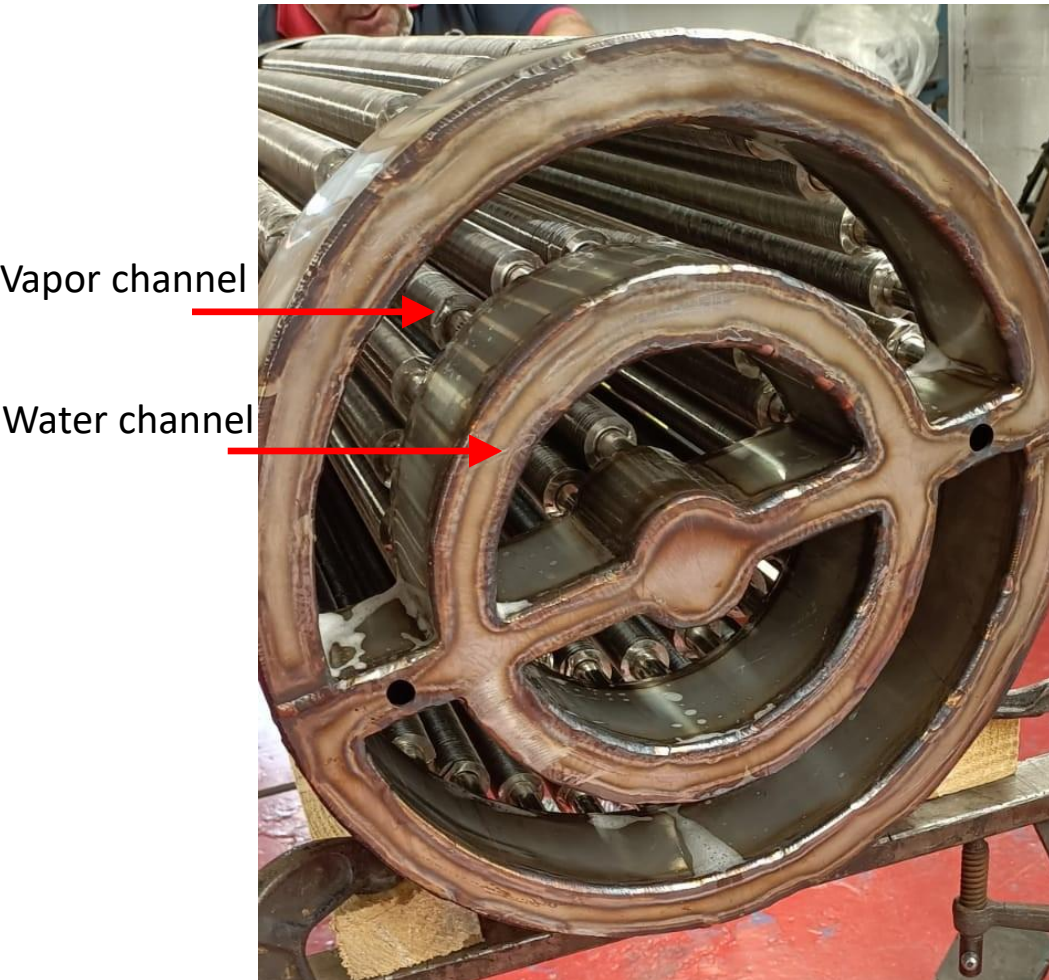
# Scaled up test rig development

8 kW capacity thermal storage rig



# Key components

Absorber tubes



Evaporator tubes





# Way forward

- Absorption and desorption performance evaluation of the thermochemical storage
- Integration analysis with heat pumps for space heating applications

## Discharging cycle

